

REMARKS

The purpose of this Preliminary Amendment is to eliminate multiple dependent claims in order to avoid the additional fee. Applicants reserve the right to reintroduce claims to canceled combined subject matter.

Attached hereto is a marked-up version of the changes made to the claims by the current amendment. The attached pages are captioned "**Version With Markings to Show Changes Made**".

Respectfully submitted,



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VERSION WITH MARKINGS TO SHOW CHANGES MADE

Claims 3 -15, 18 and 19 were amended as follows:

3. (Amended) Process according to Claim 1 ~~or 2~~, characteriszed in that the microreactor is a static micromixer.
4. (Amended) Process according to ~~one of~~ Claims 1 ~~to 3~~, characteriszed in that the microreactor is connected to a capillary, preferably a heatable capillary, via an outlet.
5. (Amended) Process according to ~~one of~~ Claims 1 ~~to 4~~, characteriszed in that the volume of the microreactor is $\leq 10 \mu\text{l}$, preferably $\leq 1 \mu\text{l}$.
6. (Amended) Process according to ~~one of~~ Claims 1 ~~to 5~~, characteriszed in that the microreactor is heatable.
7. (Amended) Process according to ~~one of~~ Claims 1 ~~to 6~~, characteriszed in that the microreactor has channels having a diameter of from 10 to 1000 μm , preferably from 20 to 800 μm , particularly preferably from 30 μm to 400 μm .
8. (Amended) Process according to ~~one of~~ Claims 1 ~~to 7~~, characteriszed in that the reaction mixture flows through the microreactor at a flow rate of from 0.1 $\mu\text{m}/\text{min}$ to 10 ml/min , preferably from 1 $\mu\text{l}/\text{min}$ to 1 ml/min .
9. (Amended) Process according to ~~one of~~ Claims 1 ~~to 8~~, characteriszed in that the residence time of the compounds employed in the microreactor, where appropriate in the microreactor and the capillaries, is ≤ 3 hours, preferably ≤ 1 hour.

10. (Amended) Process according to ~~one of Claims 1 to 9~~, characteriszed in that it is carried out at a temperature of from -90 to +150°C, preferably from -20 to +40°C, particularly preferably from -10 to +20°C.
11. (Amended) Process according to ~~one of Claims 1 to 10~~, characteriszed in that the course of the reaction is monitored by chromatography, preferably gas chromatography, and where appropriate regulated.
12. (Amended) Process according to ~~one of Claims 1 to 11~~ 1, characteriszed in that the brominated product is isolated from the reaction mixture by extraction or precipitation.
13. (Amended) Process according to ~~one of Claims 1 to 12~~, characteriszed in that the brominating reagent employed is elemental bromine, dibromoisocyanuric acid, N-bromosuccinimide, hypobromous acid, organic hypobromites, preferably trifluoroacetyl hypobromite, N-bromoacetamide, -bromophthalimide, pyridinium perbromide and/or dioxane dibromide.
14. (Amended) Process according to ~~one of Claims 1 to 13~~, characteriszed in that the catalyst employed is iodine, mineral acids, preferably sulphuric acid or nitric acid, and/or Lewis acids, preferably aluminum halides, iron halides, zinc halides or antimony halides.
15. (Amended) Process according to ~~one of Claims 1 to 14~~, characteriszed in that between 0.1 and 100 mol%, preferably between 1 and 10 mol%, of the catalyst are employed, based on the amount of organic compound employed.
18. (Amended) Bromination microreactor according to Claim ~~16 or 7~~, characteriszed in that the residence zone is a capillary, preferably a heatable capillary.
19. (Amended) Bromination microreactor according to ~~one of Claims 16 to 18~~, characteriszed in that it is heatable.